

TACONIC

136 Coonbrook Road - P.O. Box 69
Petersburgh, New York 12138
Telephone: 518-658-3202
Fax: 518-658-3204

September 30, 2005

Richard Elder
Rensselaer County Dept. of Health
County Office Bldg.
1600 7th Ave
Troy, New York 12180

RE: Taconic (manufacturing facility) of Petersburg, Rensselaer County, NY water well plumbing modifications


Dear Mr. Elder:

Taconic, formerly known as Taconic Plastics, of Petersburg, NY is a small manufacturing facility that coats woven fabrics, mainly fiberglass, with PTFE dispersions. Clearly you and Dawn Breault are very familiar with our facility. As you would expect, it is important for Taconic to review current and past practices at our facility to better understand environmental, health and safety processes/issues. Upon performing this multi-media site review, we informed your office in August 2005 the presence of an un-regulated chemical (PFOA) in the groundwater that is related to the procurement/use of PTFE at our site. As you are aware, much of our facility was already using delivered, bottled drinking water and the discovery of PFOA just extended the use of bottled water to all areas. We wish to further diminish the (un-defined) risk of incidental PFOA exposure by cleaning/polishing the well water supplied to our facility. Discussions with major PTFE industry personnel indicate the use of Granulated Activated Carbon (GAC) is very useful to sequester PFOA in the water column. Thus, attached to this letter is a permit application to add (in series) Granulated Activated Carbon (GAC) systems to our (3) wells onsite. As an added note, well #3 that supplies water to building #6/#9 (address of: 98 Coon Brook Road), also has a UV system attached to the system.

Thus, we request you review the attached application and allow our installation of the system.

Should you have any additional questions, I may be contacted at 518-658-3202.

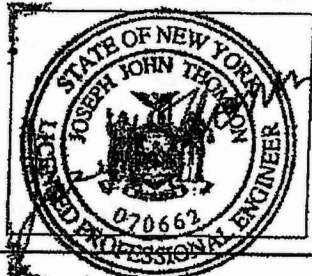
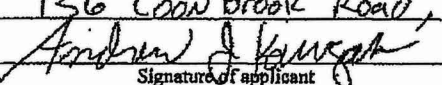
Sincerely,


Andrew Kawczak
Environmental manager

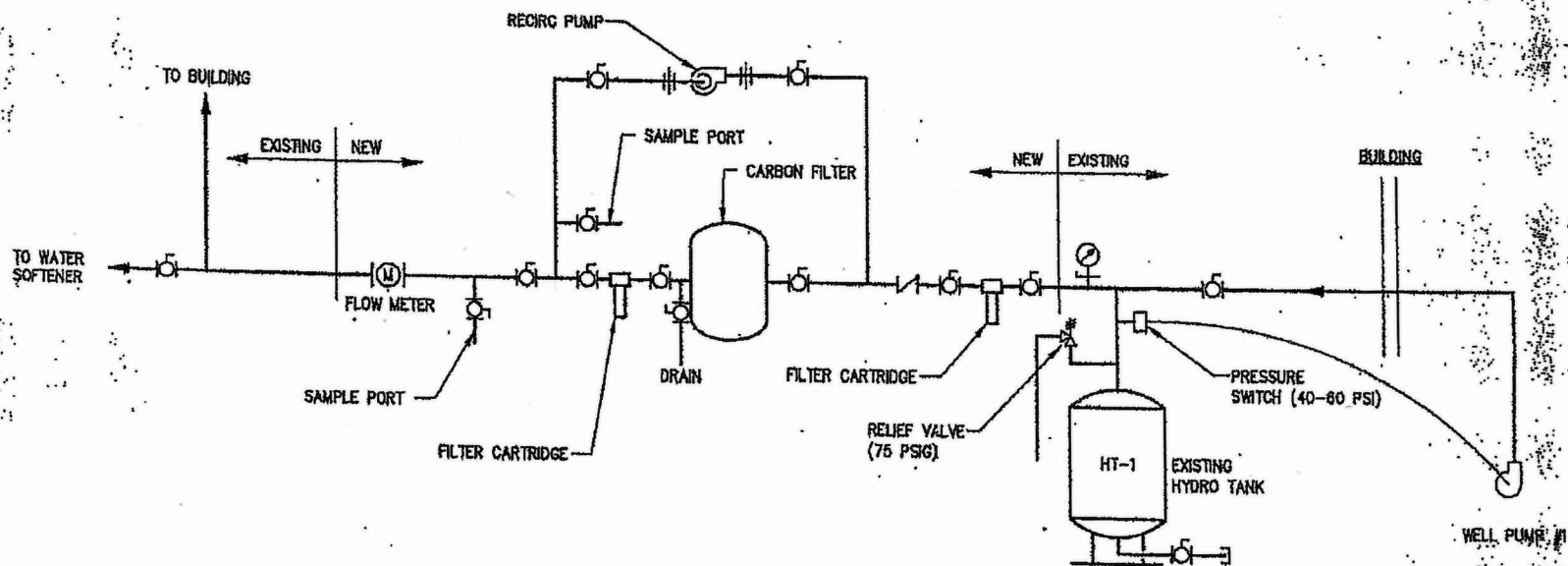
TAC EPA 04776

NEW YORK STATE DEPARTMENT OF HEALTH
Bureau of Water Supply Protection

Application for Approval of Plans for
Public Water Supply Improvement

Applicant TACONIC		Location of works (C, V, T) PETERSBURGH		County RENSSELAER	Water District (specific area served) JUST TACONIC
Type of ownership <input type="checkbox"/> Municipal <input type="checkbox"/> Commercial <input checked="" type="checkbox"/> Industrial <input type="checkbox"/> Water Works Corp.		<input checked="" type="checkbox"/> Private - Other <input type="checkbox"/> Private - Institutional <input type="checkbox"/> Board of Education		<input type="checkbox"/> Authority <input type="checkbox"/> Federal <input type="checkbox"/> State	<input type="checkbox"/> Interstate <input type="checkbox"/> International <input type="checkbox"/> Native American Reservation
<input checked="" type="checkbox"/> Modifications to existing system. If checked, provide PWS ID # NY 4118458					
New System. If checked, provide capacity development (viability) analysis*					
If this project involves a new system, new water district, or a district extension provide boundary description location details in digital format on CD or Floppy Disk. If digital boundary location details are not available provide a text description. <input type="checkbox"/> Digital GIS Data Provided <input type="checkbox"/> Digital CAD Data Provided <input type="checkbox"/> Other Digital Data Provided <input type="checkbox"/> Text Description Provided <input checked="" type="checkbox"/> N/A					
Funding Source <input checked="" type="checkbox"/> Private <input type="checkbox"/> DWSRF** <input type="checkbox"/> Federal <input type="checkbox"/> Other					
If DWSRF is checked, provide DWSRF # _____					
Estimated Project Cost Source \$ _____ Treatment \$ 6K± Storage \$ 6K± Distribution \$ _____ Pumping \$ 2K± Engineering \$ 4K± Legal/Permitting \$ _____ Total \$ 18K±					
Type of Project <input type="checkbox"/> Source <input type="checkbox"/> Corrosion Control <input type="checkbox"/> U.V. Light Disinfection <input type="checkbox"/> Distribution <input type="checkbox"/> Transmission <input checked="" type="checkbox"/> Pumping Unit <input type="checkbox"/> Fluoridation <input checked="" type="checkbox"/> Storage <input type="checkbox"/> Chlorination <input checked="" type="checkbox"/> Other Treatment <input type="checkbox"/> Other					
Project Description: INSTALL TANKS, PUMPS, GAC CONTAINERS TO provide Added water storage & WATER QUALITY IMPROVEMENTS TO (3) wells					
Population Total population of service area < 200 EMPLOYEES % population actually served 100 % population served affected by project 100					
Latest total consumption data (in MGD) EST. FROM (3) wells Avg. day 0.009 Year 2005 Max. day 0.010 Year 2005 Peak hr. 0.0016 Year 2005				14. NYS Professional Licensed Engineer Stamp & Signature *** 	
(Note: Bottled water is also provided on-site)					
Name of design engineer Robert Flores - working for Clough Harbour Assoc. Address 111 Winners Circle, Albany, NY, 12205 Telephone No. 518 453-4507 E-Mail rflores@cha-llp.com Fax No. 518 453-4773					
Name and title of applicant or designated representative ANDREW KAWCZAK WORKING FOR TACONIC, ENV. MGR. Address 136 COON BROOK ROAD, PETERSBURGH, NY 12138 Signature of applicant  Date 9/29/05					
NOTE: All applications must be accompanied by 3 sets of plans, 3 sets of specifications and an engineer's report describing the project in detail. The project must first be discussed with the appropriate city, county, district or regional public health engineer. Signature by a designated representative must be accompanied by a letter of authorization. * Additional information regarding capacity development may be found at: http://www.health.state.ny.us/nysdoh/water/main.htm ** Current DWSRF project listings may be found at: http://www.health.state.ny.us/nysdoh/water/main.htm *** By affixing the stamp and signature the Design Engineer agrees that the plans and specifications have been prepared in accordance with the most recent version of the recommended standards for water works and in accordance with the NYS Sanitary Code.					

These are (L's)



**WATER SUPPLY DETAIL
BUILDING 2**

*DESIGN IS THE SAME WELLS 2+3
WITH THE APPROPRIATE CARBON UNIT*

CHA

CLOUGH HARBOUR & ASSOCIATES LLP
11 Winans Circle, PO Box 5298, Albany, NY 12205
Phone (518) 865-6600 • www.cloughharbour.com

FIGURE-1

NO SCALE

DATE: AUGUST, 2005

CARBON TREATMENT SYSTEM

TACONIC - PETERSBURGH, NEW YORK

TAC EPA 04778

CHA

CHA COMPUTATION PAD

COMPLETED BY: L. R. BARNHART
 CHECKED BY: R. Young
 PROJECT NAME: CARBON TREATMENT SYSTEM
 PROJECT LOCATION: TACONIC

PROJECT				PHASE				ORG			
1	4	6	0	4	1	0	0	1	1	2	0

SHEET #: 1 OF 2
 DATE: 8-2-05
 SUBJECT: _____

AMOUNT OF WATER SUPPLIED BY WELLS

WELL #1 - 3 GPM
 WELL #2 - 3 GPM
 WELL #3 - 20 GPM

AMOUNT OF PFOA DETECTED IN WELLS

	PFOA CONC.
WELL #1	148/152 ng/mL = 150×10^{-9} gm / 10^{-3} L
WELL #2	117/116 ng/mL = 117×10^{-9} gm / 10^{-3} L
WELL #3	2.07/2.03 ng/mL = 2.05×10^{-9} gm / 10^{-3} L

DUPONT HAS RECOMMENDED THAT ACTIVATED CARBON
 BE USED TO REMOVE PFOA / APFO FROM WATER.

WELLS 1 + 2 :

AMOUNT OF PFOA PER GALLON BASED ON THE CONCENTRATION
 DETECTED IN WELL #1:

$$\left(150 \times 10^{-9} \text{ gm} / 10^{-3} \text{ L}\right) \left(1.0 \text{ lb} / 454 \text{ gm}\right) \left(3.78 \text{ L} / \text{GAL}\right) \\
= 1.25 \times 10^{-6} \text{ lb OF PFOA} / \text{GAL}$$

AMOUNT OF PFOA TO BE REMOVED AT 3 GPM

$$= (1.25 \times 10^{-6} \text{ lb} / \text{GAL}) (3.0 \text{ GAL} / \text{MIN}) (60 \text{ MIN} / \text{HR}) (24 \text{ HR} / \text{DAY}) \\
= 5,400 \times 10^{-6} \text{ lb OF PFOA} / \text{DAY} \\
= 5.4 \times 10^{-3} \text{ lb OF PFOA} / \text{DAY} \\
= 0.0054 \text{ lb} / \text{DAY}$$

$$1 \text{ lb OF PFOA} = 1.0 \text{ lb} / 0.0054 \text{ lb} / \text{DAY} \approx 185 \text{ DAY OF FLOW}$$

CARBON UNIT: FX-3

RECOMMENDED MAX FLOW 7 GPM
 AMOUNT OF CARBON 80 LBS.
 OR EQUIVALENT

CHA COMPUTATION PAD

1	4	6	0	4	1	0	1	1	2	0	2
PROJECT											
PHASE											
ORG											
SHEET # 2 OF 2											
DATE 8-2-85											
SUBJECTS											

COMPLETED BY: L. R. BILLYMUS	PROJECT NAME: CARBON TREATMENT SYS.	PROJECT LOCATION: TACONIC
CHECKED BY: R. YODER		



Well #3:

Amount of PFOA BEING ELIMINATED:

$$= [(0.05 \times 10^{-9} \text{ gm}/10^{-3} \text{ L})(3.78 \text{ L/gal})] / 45 \text{ gm}/14$$

$$= 0.017 \times 10^{-6} \text{ lb of PFOA/gal}$$

Amount of PFOA to be removed at 20 ppm

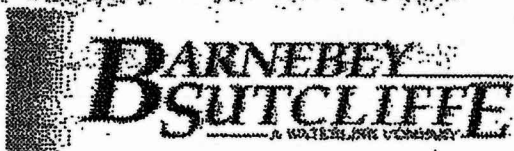
$$= (0.017 \times 10^{-6} \text{ lb/gal}) \times (80 \text{ gal/min}) \times (60 \text{ min/hr}) \times (24 \text{ hr/day})$$

$$= 489.6 \times 10^{-6} \text{ lb/day}$$

$$= 0.00049 \text{ lb/day}$$

1 lb of PFOA = 1.0 lb / 0.00049 lb/day = 2040 days or 5.6

CARBON UNIT: FX-7 RECOMMENDED MAX. FLOW 25 GPM
 AMOUNT OF CARBON 180 lbs, on EQUIPMENT



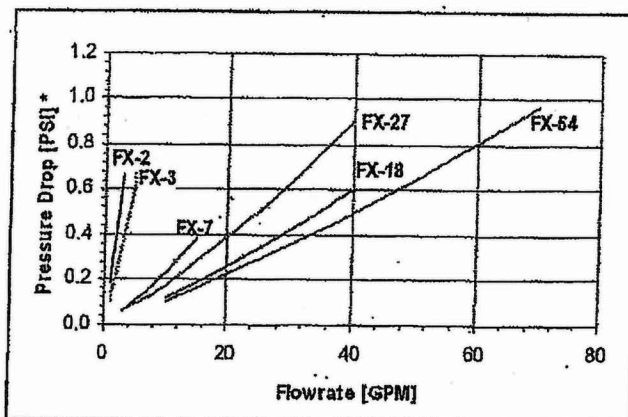
*Powerful Solutions
for a New Tomorrow*

Protect FX Series

The Protect FX series vessels are designed as lightweight, non-corrosive pressure vessels, and are well suited for most harsh chemical environments. They can operate at flow rates from 3 to 70 gpm, a maximum pressure of 150 psi, and maximum temperature of 140 °F.

Important Features:

- 150 PSI @ 120 °F design pressure
- Fiberglass reinforced plastic construction
- Polyethylene inner shell
- Skirt or rubber tripod base depending on size
- Lower PVC laterals positioned for superior distribution, eliminates need for media support bed
- Rust-prohibitive exterior coating
- Chemical resistant internal liner



* Estimated pressure drop based on 8x30 mesh carbon.

Model #	GAC		Recommended Maximum Flow Rate, gpm	Weight, lbs. (Empty / Operating)
	ft. ³	lbs.**		
FX-2	1.8	50	4	20 / 70
FX-3	2.8	80	7	30 / 110
FX-7	6.5	180	25	90 / 270
FX-18	18	500	50	370 / 870
FX-27	27	750	50	370 / 1,120
FX-54	54	1,500	100	700 / 2,200

** Weight estimated from vessel volume.

Corporate Capabilities:

Barnbey Sutcliffe has been manufacturing and servicing adsorption equipment for over 80 years. Some of our other products and services include:

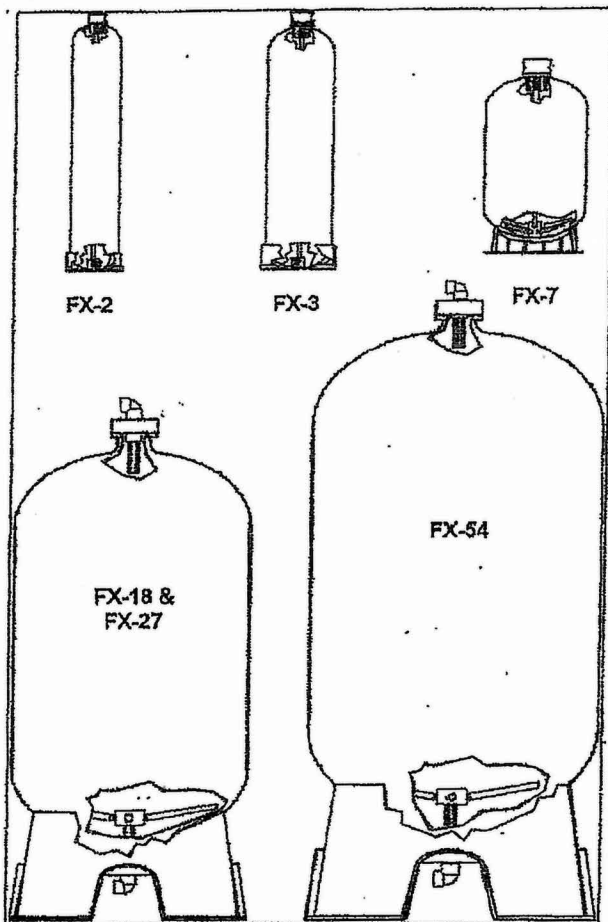
- Wide variety of coal & coconut shell carbons
- Broad range of filtration media
- National network of service centers
- Carbon reactivation (hazardous & non-hazardous)
- Vessel rental
- The industry's largest line of NSF certified carbons
- Spent media exchange
- Technical support
- Custom-engineered systems
- ASME Code-certified fabrication facility

835 N. Cassady Ave. • Columbus, OH 43219 • 1-800-888-2272 • 614-258-9501 • Fax 614-258-3464 • E-mail: activated_carbon@waterlink.com • www.bsccarbon.com
 Rocky Mountain Office • Reno, NV • 775-355-7770 • Fax 775-355-7785 / Western Regional Office • Los Angeles, CA • 562-802-3400 • Fax 562-802-3480
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BARNEBEY BUTCLIFFE

A WATTSGLAZIER COMPANY

Powerful Solutions
Join A New Tomorrow



Available Options:

- ASME code stamp
- Vacuum relief valve
- Higher pressure available
- With or without internals
- Custom colors
- Pressure indicators
- Side mounted Inlet / outlet
- Custom sizes
- Sight glasses
- Extended, tripod, or bolted base
- Lifting lugs
- Prepped automatic systems

To discuss your application needs, call us at one of our regional offices or at

1-800-866-2272

www.bscarbons.com

Overall height measured to top of head for FX-2, FX-3, FX-7. Overall height measured to top of elbow for FX-18, FX-27, & FX-54. Drawings not to scale.

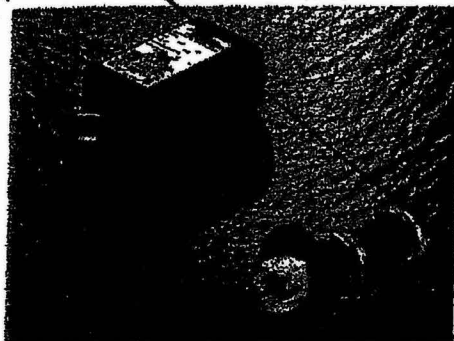
Model	Vessel O.D.	Overall Height	Inlet / Outlet	Base Type	Base O.D.
FX-2	10"	56" ±	¾" fpt	Skirt	10 ¼" ±
FX-3	13 ½"	57" ±	1" fpt	Skirt	13 ½" ±
FX-7	24 ½"	44" ±	1" fpt	Stand Base	20 ½" ±
FX-18	36 ½"	94" ±	2" socket	Tripod	36 ¾" ±
FX-27	36 ½"	94" ±	2" socket	Tripod	36 ¾" ±
FX-54	49"	100" ±	2" socket	Tripod	47 ½"

Barnebey Butcliffe is continually improving carbon capacity and system performance. Due to the ongoing improvement of our products, we reserve the right to change system specifications and performance criteria without notification.

835 N. Cassady Ave. • Columbus, OH • 43219 • 1-800-866-2272 • 614-258-8501 • Fax 614-258-3464 • E-mail: sativated_carbon@waterlink.com • www.bscarbons.com
 Rocky Mountain Office • Reno, NV • 775-355-7770 • Fax 775-355-7785 / Western Regional Office • Los Angeles, CA • 562-802-3400 • Fax 562-802-3450
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TAC EPA 04782

Model 003 Cartridge Circulator



Model Nomenclature

- B — Bronze, Sweat
- BC — Bronze, Sweat, Panel Mount Tappings
- BT — Bronze, Threaded
- BC-I — Bronze, Union, Panel Mount Tappings

Performance Data

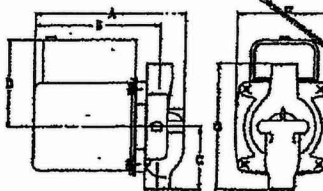
Flow Range: 0 — 6 GPM
Head Range: 0 — 5 Feet
Connection Sizes: 1/2" Swt, 3/4" Swt, 3/4" NPT, 1" Union

Application

The Taco 003 is designed for circulating hot or chilled fresh water in open or closed loop, lower flow applications. Flow characteristics are ideal for Domestic Hot Water Recirculation, Heat Recovery Units, Water Source Heat Pumps, and Potable Water Systems. The unique, replaceable cartridge contains all of the moving parts and allows for easy service instead of replacing the entire circulator. The compact, low power consumption design is ideal for high efficiency jobs.

Pump Dimensions & Weights

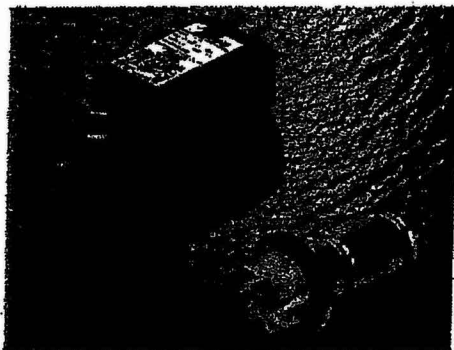
Model	Connection	A		B		C		D		F		G		Ship Wt.	
		in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	lbs.	Kg
003-B4	1/2" Swt	5-1/8	130	4-1/8	105	2-3/16	56	3-1/16	78	3-5/16	84	4-13/32	112	6.0	2.7
003-BC4	1/2" Swt	5-1/8	130	4-1/8	105	2-1/8	54	3-1/16	78	3-5/16	84	4-1/4	108	6.0	2.7
003-BT4	3/4" NPT	5-5/8	143	4-7/8	124	2	51	3-1/16	78	3-5/16	84	4	102	6.0	2.7
003-BC4-I	1" Union	5-5/32	131	4-11/32	110	2-31/32	76	3-1/16	78	3-5/16	84	5-15/16	151	6.0	2.7



Electrical Data

Model	Volts	Hz	Ph	Amps	RPM	HP
003 All Models	115	60	1	.43	3250	1/40
Motor Type	Permanent Split Capacitor Impedance Protected					
Motor Options	220/50/1, 220/60/1, 230/60/1, 100/110/50/60/1					

Model 006 Cartridge Circulator



Model Nomenclature

- B — Bronze, Sweat
- BC — Bronze, Sweat, Panel Mount Tappings
- BT — Bronze, Threaded
- BC-I — Bronze, Union, Panel Mount Tappings

Performance Data

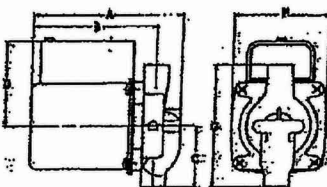
Flow Range: 0 — 10 GPM
Head Range: 0 — 9 Feet
Connection Sizes: 1/2" Swt, 3/4" Swt, 3/4" NPT, 1" Union

Application

The Taco 006 is designed for circulating hot or chilled fresh water in open or closed loop, lower flow applications. Typical uses include Domestic Hot Water Recirculation, Hydro-Air Heating/Cooling, Heat Recovery Units, Water Source Heat Pumps, Drain Down Open Loop Solar systems and Potable Water applications. The unique, replaceable cartridge contains all of the moving parts and allows for easy service instead of replacing the entire circulator. The compact, low power consumption design is ideal for high efficiency jobs.

Pump Dimensions & Weights

Model	Connection	A		B		C		D		F		G		Ship Wt.	
		in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	lbs.	Kg
006-B4	3/4" Swt	5-1/8	130	4-1/8	105	2-3/16	56	3-1/16	78	3-5/16	84	4-13/32	112	6.0	2.7
006-BC4	1/2" Swt	5-1/8	130	4-1/8	105	2-1/8	54	3-1/16	78	3-5/16	84	4-1/4	108	6.0	2.7
006-BT4	3/4" NPT	5-5/8	143	4-7/8	124	2	51	3-1/16	78	3-5/16	84	4	102	6.0	2.7
006-BC4-I	1" Union	5-5/32	131	4-11/32	110	2-31/32	76	3-1/16	78	3-5/16	84	5-15/16	151	6.0	2.7



Electrical Data

Model	Volts	Hz	Ph	Amps	RPM	HP
006 All Models	115	60	1	.52	3250	1/40
Motor Type	Permanent Split Capacitor Impedance Protected					
Motor Options	220/50/1, 220/60/1, 230/60/1, 100/110/50/60/1					

Model 005 Cartridge Circulator



Model Nomenclature

F - Cast Iron, Flanged

BF - Bronze, Flanged

Variations:

Z - Zoning Circulator

J - Bronze Cartridge with Cast Iron Casing

Performance Data

Flow Range: 0 - 18 GPM

Head Range: 0 - 9.5 Feet

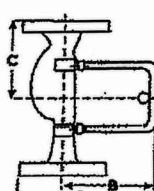
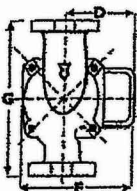
Connection Sizes: 3/4", 1", 1-1/4", 1-1/2" Flanged

Application

The Taco 005 is designed for a wide range of Residential/Light Commercial water circulating applications. Typical uses include Hydronic heating, add a zone additions, Zoning with circulators, Chilled Water cooling and Domestic Water Systems. Available in Cast Iron or Bronze construction with universal flange to flange dimensions. The unique replaceable cartridge contains all of the moving parts and allows for easy service, instead of replacing the entire circulator. Compact, direct-drive, low power consumption design is ideal for high efficiency jobs.

Pump Dimensions & Weights

Model	Casing	A		B		C		D		F		G		Ship Wt.	
		in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	lbs.	Kg
005-F2	Cast Iron	5-5/8	143	4	102	3-3/16	81	2-15/16	75	4-3/4	121	6-3/8	162	8.0	3.6
005-BF2	Bronze	5-5/8	143	4	102	3-3/16	81	2-15/16	75	4-3/4	121	6-3/8	162	8.0	3.6



Electrical Data

Model	Volts	Hz	Ph	Amps	RPM	HP
005-F2	115	60	1	.53	3250	1/35
005-BF2	115	60	1	.54	3250	1/35
Motor Type	Permanent Split Capacitor Impedance Protected					
Motor Options	220/50/1, 220/60/1, 230/60/1, 100/110/50/60/1					

Model 007 Cartridge Circulator



Model Nomenclature

F - Cast Iron, Flanged

BF - Bronze, Flanged

Variations:

Z - Zoning Circulator

J - Bronze Cartridge with Cast Iron Casing

Performance Data

Flow Range: 0 - 20 GPM

Head Range: 0 - 11 Feet

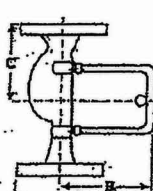
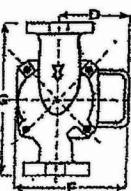
Connection Sizes: 3/4", 1", 1-1/4", 1-1/2" Flanged

Application

The Taco 007 is a cartridge style, maintenance free, wet-rotor, in-line, single stage circulator. It is designed for quiet operation in Hydronic Heating, Radiant Heating, Hydro-Air Fan Coils, Indirect Water Heating, Chilled Water cooling, and Domestic Water Systems. Available in Cast Iron or Bronze construction with universal flange to flange dimensions. The unique replaceable cartridge contains all of the moving parts and allows for easy service, instead of replacing the entire circulator. Ideal for a wide range of applications.

Pump Dimensions & Weights

Model	Casing	A		B		C		D		F		G		Ship Wt.	
		in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	in.	mm	lbs.	Kg
007-F5	Cast Iron	6-1/8	156	4-1/2	114	3-3/16	81	2-15/16	75	4-3/4	121	6-3/8	162	8.0	3.6
007-BF5	Bronze	6-1/8	156	4-1/2	114	3-3/16	81	2-15/16	75	4-3/4	121	6-3/8	162	8.0	3.6



Electrical Data

Model	Volts	Hz	Ph	Amps	RPM	HP
007-F5	115	60	1	.70	3250	1/25
007-BF5	115	60	1	.76	3250	1/25
Motor Type	Permanent Split Capacitor Impedance Protected					
Motor Options	220/50/1, 220/60/1, 230/60/1, 100/110/50/60/1					



Wastewater Technology Fact Sheet

Granular Activated Carbon Absorption and Regeneration

DESCRIPTION

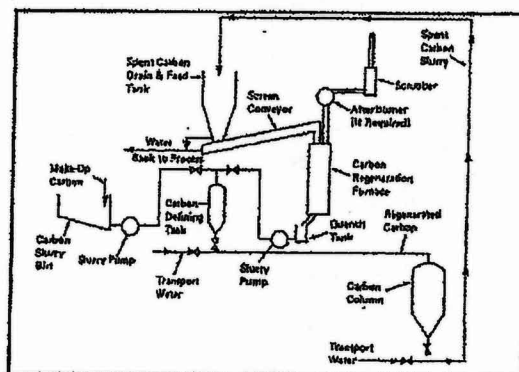
Granular activated carbon (GAC) absorption has been used successfully for the advanced (tertiary) treatment of municipal and industrial wastewater. GAC is used to adsorb the relatively small quantities of soluble organics (See Table 1) and inorganic compounds such as nitrogen, sulfides, and heavy metals remaining in the wastewater following biological or physical-chemical treatment. Adsorption occurs when molecules adhere to the internal walls of pores in carbon particles produced by thermal activation.

**TABLE 1 ORGANIC COMPOUNDS
AMENABLE TO ABSORPTION BY GAC**

Class	Example
Aromatic solvents	Benzene, toluene, xylene
Polynuclear aromatics	Naphthalene, biphenyl
Chlorinated aromatics	Chlorobenzene, PCBs, endrin, toxaphene, DDT
Phenolics	Phenol, cresol, resorcinol, nitrophenols, chlorophenols, alkyl phenols
Aromatic amines & high molecular weight aliphatic amines	Aniline, toluene diamine
Surfactants	Alkyl benzene sulfonates
Soluble organic dyes	Methylene blue, textiles, dyes
Fuels	Gasoline, kerosene, oil
Chlorinated solvents	Carbon tetrachloride, perchloroethylene
Aliphatic & aromatic acids	Tar acids, benzoic acids
Pesticides/herbicides	2,4-D, atrazine, simazine, aldicarb, alachlor, carbofuran

Source: U.S. EPA, 1984.

GAC systems are generally composed of carbon contactors, virgin and spent carbon storage, carbon transport systems, and carbon regeneration systems (See Figure 1). The carbon contactor consists of a lined steel column or a steel or concrete rectangular tank in which the carbon is placed to form a "filter" bed. A fixed bed downflow column contactor (See Figure 2) is often used to contact wastewater with GAC. Wastewater is applied at the top of the column, flows downward through the carbon bed, and is withdrawn at the bottom of the column. The carbon is held in place with an underdrain system at the bottom of the contactor. Provisions for backwash and surface wash of the carbon bed are required to prevent buildup of excessive headloss due to accumulation of solids and to prevent the bed surface from clogging.

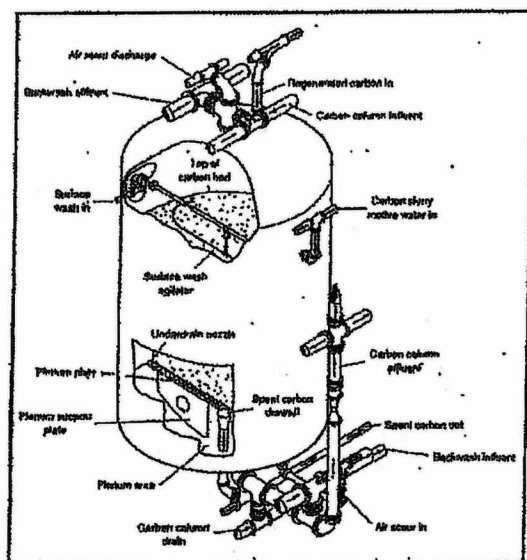


Source: WEF MOP 8, 1998.

**FIGURE 1 GAC ADSORPTION
SCHEMATIC**

Expanded bed and moving bed carbon contactors have been developed to overcome problems associated with headloss buildup experienced with fixed bed downflow contactors. In an expanded bed system, wastewater is introduced at the bottom of the contactor and flows upward, expanding the carbon bed, much as the bed expands.

during backwash of a fixed bed downflow contactor. In the moving bed system, spent carbon is replaced continuously so that the headloss does not build up. Carbon contactors may be operated under either pressure or gravity flow. The choice between pressure and gravity flow generally depends on the available pressure (head) within the wastewater treatment plant and cost.



Source: Tchobanoglous and Burton, 1991.

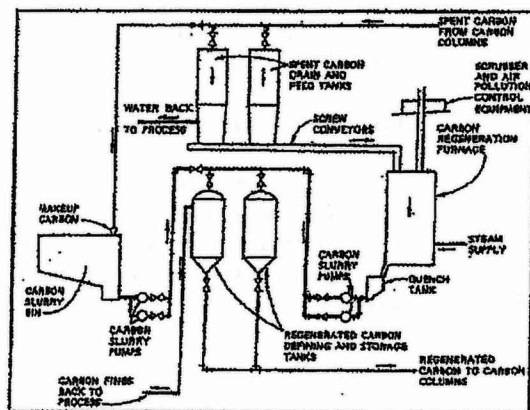
FIGURE 2 TYPICAL DOWNFLOW CARBON CONTACTOR

All carbon contactors must be equipped with carbon removal and loading mechanisms to allow spent carbon to be removed and virgin or regenerated carbon to be added. Spent, regenerated, and virgin carbon is typically transported hydraulically by pumping as a slurry. Carbon slurries may be transported with water or compressed air, centrifugal or diaphragm pumps, or eductors.

When the carbon contactor effluent quality reaches minimum water quality standards, the spent carbon is removed from the contactor for regeneration. Small systems usually find regeneration of their spent carbon at an off-site commercial reactivation facility to be the most convenient and economical method. In this case, the spent carbon is hydraulically transported from the contactor to a

waiting truck. Regenerated or virgin carbon is then hydraulically transported from a second truck or from a separate compartment in the first truck to the contactor, then to a commercial reactivation facility. Generally, systems which contain at least one million pounds of carbon find on-site regeneration to be cost effective.

Carbon regeneration is accomplished primarily by thermal means. Organic matter within the pores of the carbon is oxidized and thus removed from the carbon surface. The two most widely used regeneration methods are rotary kiln and multiple hearth furnaces. Approximately 5 to 10 percent of the carbon is destroyed in the regeneration process or lost during transport and must be replaced with virgin carbon. The capacity of the regenerated carbon is slightly less than that of virgin carbon. Repeated regeneration degrades the carbon particles until an equilibrium is eventually reached providing predictable long term system performance. See Figure 3 for a schematic of the carbon regeneration process.



Source: WEF MOP 8, 1998

FIGURE 3 REGENERATION SCHEMATIC

APPLICABILITY

Typically, GAC adsorption is utilized in wastewater treatment as a tertiary process following conventional secondary treatment or as one of several unit processes composing physical-chemical

treatment. In wastewater treatment plants utilizing biological secondary treatment, GAC adsorption is generally located after filtration and prior to disinfection. When utilized in a physical-chemical treatment process, GAC adsorption is generally located following chemical clarification and filtration and prior to disinfection. In addition, GAC adsorption systems have a relatively small footprint making them suitable for facilities with limited land availability.

The successful application of carbon adsorption for municipal wastewater treatment depends on the quality and quantity of the wastewater delivered to the adsorption system. For a carbon contactor to perform effectively, the feed water to the unit should be of uniform quality (suspended solids concentrations less than 20 mg/l) and without surges in flow. Wastewater constituents that may adversely affect carbon adsorption include suspended solids, BOD₅, and organics such as methylene blue active substances or phenol and dissolved oxygen. Environmental factors that must be considered include pH and temperature because they may impact solubility, which affects the adsorption properties of the wastewater components onto carbon (WEF MOP 8, 1998).

ADVANTAGES AND DISADVANTAGES

Before deciding whether carbon adsorption/regeneration meets the needs of a municipality, it is important to understand the advantages and disadvantages of both the adsorption and regeneration process.

Advantages (Adsorption)

- For wastewater flows which contain a significant quantity of industrial flow, GAC adsorption is a proven, reliable technology to remove dissolved organics.
- Space requirements are low.
- GAC adsorption can be easily incorporated into an existing wastewater treatment facility.

Advantages (Regeneration)

- Systems are reliable from a process standpoint.
- Reduces solid waste handling problems caused by the disposal of spent carbon.
- Saves up to 50 percent of the carbon cost.

Disadvantages (Adsorption)

- Under certain conditions, granular carbon beds may generate hydrogen sulfide from bacterial growth, creating odors and corrosion problems.
- Spent carbon, if not regenerated, may present a land disposal problem.
- Wet GAC is highly corrosive and abrasive.
- Requires pretreated wastewater with low suspended solids concentration. Variations in pH, temperature, and flow rate may also adversely affect GAC adsorption.

Disadvantages (Regeneration)

- Air emissions from the furnace contain volatiles stripped from the carbon. Carbon monoxide is formed as a result of incomplete combustion. Therefore, afterburners and scrubbers are usually needed to treat exhaust gases.
- The induced draft fan of a multiple hearth furnace may produce a noise problem.
- The process is most effective when operated on a 24-hour basis, requiring around-the-clock operator attention.
- The process is subject to more mechanical failures than other wastewater treatment processes.

DESIGN CRITERIA

Prior to the design of GAC systems, a pilot plant study should be performed to determine if the technology will meet discharge permit requirements and to quantify optimum flow rate, bed depth, and operating capacity on a particular wastewater. This information is required to determine the dimensions and number of carbon contactors required for continuous treatment.

The sizing of carbon contactors is based on contact time, hydraulic loading rate, carbon bed depth, and number of contactors. The carbon contact time typically ranges from 15 to 35 minutes depending on the application, wastewater constituents and desired effluent quality. Hydraulic loading rates of 4 to 10 gpm/sq.ft are typically used for upflow carbon columns. For downflow carbon columns, hydraulic loading rates of 3 to 5 gpm/sq.ft are used. Carbon bed depth varies typically within a range of 10 to 40 feet depending on carbon contact time (Tchobanoglous, 1991).

The number of contactors should be sufficient to ensure enough carbon contact time to maintain effluent quality while one column is off line during removal of spent carbon or maintenance. The normal practice is either to use two columns in series and rotate them as they become exhausted or to use multiple columns in parallel so that when one column becomes exhausted, the effluent quality will not be significantly affected (WEF MOP 8, 1998).

Regeneration facilities are typically sized based on carbon dosage or use rate. The dosage rate depends on the strength of the wastewater applied to the carbon and the required effluent quality. Typical dosage rates for filtered, secondary effluent range from 400 to 600 lbs/mil.gall., while typical dosage rates for coagulated, settled and filtered raw wastewater (physical-chemical) range from 600 to 1800 lbs/mil.gall.

PERFORMANCE

Niagara Falls Wastewater Treatment Plant
Niagara Falls, New York

The Niagara Falls Wastewater Treatment Plant (NFWTP) has been operating as a physical-chemical activated carbon secondary treatment facility since 1985. With a design average daily flow capacity of 48 mgd, it is the largest municipal physical-chemical activated carbon wastewater treatment plant in operation in the United States. The treatment process consists of chemically assisted primary sedimentation, granular activated carbon adsorption, oxidation, and disinfection. The influent pH can be adjusted to compensate for industrial discharge. The current average daily flow is 35 mgd. Industrial flow to the plant is approximately 17 percent of the total flow.

The activated carbon system at NFWTP includes 28 carbon beds which are 17.3 feet wide by 42 feet long. Each carbon bed is approximately 8.5 feet in depth and contains 180,000 pounds of carbon. Primary effluent percolates downward by gravity through the GAC bed. Each carbon bed provides chemical adsorption of pollutants from the wastewater, physical filtration of solids, and biological degradation from the incidental anaerobic activity that occurs within.

The carbon beds at NFWTP operate in parallel. During dry weather, there are typically 17 carbon beds in operation with a primary effluent application rate of approximately 2.2 gpm/sq.ft. During wet weather, additional beds are placed in operation. All beds are operated at an application rate of approximately 3 gpm/sq.ft (Roll, 1996). Backwash of the carbon beds is based on headloss.

Regeneration of the spent carbon is performed on-site in a multiple hearth furnace. Each filter bed is separately removed from service and emptied of carbon. The carbon is fed to the furnace at a rate of about 2,000 lbs/hr. The regenerated carbon is kept in storage until an empty bed becomes available. Normal operating losses, which average 5.5 percent, require the addition of virgin carbon to maintain inventory levels. At present, the four month regeneration process to regenerate all of the carbon is performed once per year.

Three storage tanks are used during on-site regeneration. The spent carbon storage tank has a capacity of 2.5 carbon beds; the regenerated carbon

storage tank can hold 1.5 beds of carbon and the virgin carbon storage tank has a capacity of 1 carbon bed. Carbon is moved about the plant in a slurry through an eductor system.

With GAC adsorption, the NFWTP has achieved very low effluent organic compound concentrations. On a daily basis, the facility receives approximately 800 pounds of influent priority pollutants which are reduced by the treatment process to 12 pounds in the effluent to the Niagara River. The effluent discharge permit issued to NFWTP by the New York State Department of Environmental Conservation includes effluent limitations for volatile compounds, acid compounds, base/neutral compounds, pesticides, metals, and cyanide.

**Millard H. Robbins Reclamation Facility,
Upper Occoquan Sewerage Authority,
Centreville, Virginia**

The Millard H. Robbins Reclamation Facility (MHRRF) provides biological, tertiary treatment to an average daily wastewater flow of 24 mgd. Industrial flow to the plant is approximately 10 percent of the total flow. The treatment process consists of primary sedimentation, conventional activated sludge with nitrification, lime addition for phosphorous removal, clarification, two-stage recarbonization, flow equalization, multimedia filtration, GAC adsorption, post filtration and disinfection. The MHRRF discharges its effluent to Bull Run which flows into the Occoquan Reservoir. This reservoir serves as raw water storage for the potable water supply to portions of northern Virginia.

The activated carbon system at MHRRF includes 32 upflow carbon columns which are 10 feet in diameter and 40 feet tall. Each column has a capacity of 1mgd and contains approximately 75,000 pounds of carbon. Flow is pumped through the columns by a pump station which also serves the multimedia filters and post filtration system. Post filtration is provided following the GAC columns to remove carbon fines from the effluent to maintain the Virginia Pollutant Discharge Elimination System (VPDES) permit requirement for turbidity of 0.5 NTU.

The carbon columns at MHRRF are operated in parallel. During average daily flow periods, approximately 24 columns are in operation with the remaining eight columns brought on line during daily peak flow periods. During wet weather, flows in excess of 32 mgd are stored in a 90 million gallon pond.

Regeneration of the spent carbon is performed on-site in a multiple hearth furnace. The regeneration process takes approximately 8 to 10 weeks to regenerate approximately one-third of the carbon in all 32 columns and is performed twice each year. Consequently, it takes approximately 18 months (three regeneration cycles) to regenerate the total quantity of carbon in the columns. Spent carbon is removed from the bottom of each column and transported to the regeneration furnace through an eductor system. The regenerated carbon is then added at the top of each column. The cost for on-site regeneration at MHRRF is approximately \$0.35 per pound. Normal operating losses, which average 5 to 7 percent of the total quantity of GAC in use, require the addition of virgin carbon to maintain inventory levels. Most of the carbon attrition occurs during regeneration with approximately 10 to 12 percent of the total carbon regenerated lost during the regeneration process. Carbon is moved about the plant in a slurry through an eductor system.

GAC adsorption is utilized at MHRRF to remove non-biodegradable, soluble organics. COD is used as the surrogate indicator of non-biodegradable organics removal by the GAC columns. Currently, the Virginia Pollutant Discharge Elimination System (VPDES) discharge permit limit for COD is 10 mg/l. Following GAC regeneration, effluent COD concentrations range from 6 to 7 mg/l, which corresponds to approximately 50 percent removal of COD. As the GAC in the columns becomes exhausted, the percentage removal of COD declines to approximately 25 percent. When the effluent COD concentration has increased to 9 mg/l, GAC regeneration is initiated.

OPERATION AND MAINTENANCE

The proper operation and maintenance of GAC adsorption and regeneration systems ensures the

efficient removal of soluble organics from secondary effluent. A routine O&M schedule following manufacturer's recommendations should be developed and implemented for any GAC adsorption and regeneration system. Regular O&M includes the following:

- Backwash of carbon contactor based on headloss or flow.
- Flush carbon transport piping to prevent clogging.
- Backwash frequently after loading carbon to minimize clogging of backwash nozzles by carbon fines.
- Store an adequate supply of spent carbon to allow continuous operation of the regeneration furnace.
- Test and calibrate instrumentation and controls on a routine basis.

COSTS

The construction and operation and maintenance costs of carbon adsorption and regeneration depend on the characteristics of the wastewater to be treated, the capacity of the plant, and the plant site. Therefore, the designer is responsible for selecting a system that will meet the National Pollutant Discharge Elimination System NPDES permit requirements at the lowest cost possible. Once the optimum flow rate, bed depth, and operating capacity of GAC for a particular wastewater are determined, comparative costs for different carbon contactor configurations and the cost of on-site regeneration versus off-site regeneration can be estimated. Following a thorough engineering and economic analysis of alternatives, the final equipment configuration can be selected.

Construction costs include the carbon contactors, carbon transport system, carbon storage tanks, carbon regeneration system (if applicable), influent wastewater pumps (if applicable), and contactor backwash system. Operation and maintenance costs include the purchase of virgin carbon, on-site regeneration or purchase of regenerated carbon,

electrical power to operate pumps and controls; flushing of carbon slurry piping, and replacement of parts. Currently, the cost of virgin carbon ranges from \$0.70 to \$1.20 per pound and the cost to purchase regenerated carbon ranges from \$0.50 to \$0.78 per pound.

Operational costs depend on the characteristics of the influent wastewater and the adsorption capacity of the GAC. For example, influent wastewater which contains suspended solids concentrations greater than 20 mg/l will require more frequent backwashing of the contactor to prevent clogging of the carbon bed.

REFERENCES

Other Related Fact Sheets

Other EPA Fact Sheets can be found at the following web address:
<http://www.epa.gov/owmitnet/mtbfact.htm>

1. "Activated Carbon Adsorption & Adsorption." [http://www.scana.com/sce%26g/business_solutions/technology/ewtwaca.htm].
2. Culp, Russel L., Wesner, George Mack, and Culp, Gordon L., 1978. *Handbook of Advanced Wastewater Treatment*, 2nd Ed. Van Nostrand Reinhold Co., NY.
3. Naylor, William F. and Rester, Dennis O., 1995. Determining Activated Carbon Performance. *Pollution Engineering*, July 1.
4. Perrich Jerry R., 1981. *Activated Carbon Adsorption for Wastewater Treatment*, CRC Press, FL.
5. Roll, Richard and Crocker, Douglas, "Evolution Of A Large Activated Carbon Secondary Treatment System", WEFTEC, 1996, WEF Annual Conference, Dallas.

6. Tchobanoglous, George and Burton, Franklin L., 1991. *Wastewater Engineering, Treatment, Disposal, Reuse*, Metcalf and Eddy Inc., 3rd Ed.
7. U.S. EPA, 1984. Granular Activated Carbon Systems Problems and Remedies, U.S. EPA 800/490/9198, U.S. EPA, Washington, D.C.
8. Water Environment Federation, *Design of Municipal Wastewater Treatment Plants*, MOP No. 8, 1998.

ADDITIONAL INFORMATION

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RENSSELAER COUNTY DEPARTMENT of HEALTH

Kathleen M. Jimino
County Executive



Denise M. Ayers, M.S., F.N.P.
Public Health Director

Andrew Kawczak, Environmental Manager
C/o Taconic Plastics
136 Coonbrook Road
PO Box 69
Petersburgh, NY 12138

RE: Taconic (manufacturing facility) of Petersburgh, NY
Water Well Plumbing Modifications

Dear: Mr. Kawczak;

We have received and approved the plans to the above referenced project. Attached is a copy of the signed approval form along with the stipulations.

Please take special note of all conditions associated with this approval. In addition, please advise me when the construction begins so that I can make at least one on-site visit during the construction phase.

If there are any questions please feel free to contact me at 518-270-2644. My office hours are Monday-Friday from 8:00 am to 4:00 pm.

Thank you,


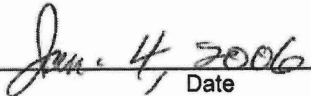
Richard Elder
Public Health Engineer

Attachments: (1)

Cc: Kevin Forcinella, Public Health Technician
File

Approval of Plans for Public Water Supply Improvement

This approval is issued under the provisions of 10 NYCRR, Part 5:

1. Applicant Taconic	2. Location of Works (C,V,T) Town of Petersburg	3. County Rensselaer	4. Water District (Specific Area Served) Taconic
5. Type of Project			
<input type="checkbox"/> 1. Source	<input checked="" type="checkbox"/> 4. Chlorination/UV	<input type="checkbox"/> 7. Storage	
<input type="checkbox"/> 2. Transmission	<input type="checkbox"/> 5. Fluoridation	<input checked="" type="checkbox"/> 8. Distribution	
<input type="checkbox"/> 3. Pumping Units	<input checked="" type="checkbox"/> 6. Other Treatment	<input type="checkbox"/> 9. Other	
Remarks: Installation of GAC filters and UV Disinfection on all three wells.			
By initiating improvement of the approved supply, the applicant accepts and agrees to abide by and conform with the following:			
<ul style="list-style-type: none">a. THAT the proposed works be constructed in complete conformity with the plans and specifications approved this day or approved amendments thereto.b. THAT the proposed works not be placed into operation until such time as a Completed Works Approval is issued in accordance with Part 5 of the New York State Sanitary Code.c. THAT this approval is granted subject to any and all applicable State, Local, and Municipal Laws, Ordinances, Codes, Rules and Regulations.d. THAT this approval is valid for (1) year from date of signature and is renewable at that time.			
ISSUED FOR THE STATE COMMISSIONER OF HEALTH			
 _____, P.E. Designated Representative		 _____ Date	
CHARLES DEFAZIO, PE Name and Title (print)		